

## Review article

## Challenges and opportunities for hydrogen production from microalgae

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## Summary

The global population is predicted to increase from ~7.3 billion to over 9 billion people by 2050. Together with rising economic growth, this is forecast to result in a 50% increase in fuel demand, which will have to be met while reducing carbon dioxide (CO<sub>2</sub>) emissions by 50–80% to maintain social, political, energy and climate security. This tension between rising fuel demand and the requirement for rapid global decarbonization highlights the need to fast-track the coordinated development and deployment of efficient cost-effective renewable technologies for the production of CO<sub>2</sub> neutral energy. Currently, only 20% of global energy is provided as electricity, while 80% is provided as fuel. Hydrogen (H<sub>2</sub>) is the most advanced CO<sub>2</sub>-free fuel and provides a 'common' energy currency as it can be produced via a range of renewable technologies, including photovoltaic (PV), wind, wave and biological systems such as microalgae, to power the next generation of H<sub>2</sub> fuel cells. Microalgae production systems for carbon-based fuel (oil and ethanol) are now at the demonstration scale. This review focuses on evaluating the potential of microalgal technologies for the commercial production of solar-driven H<sub>2</sub> from water. It summarizes key global technology drivers, the potential and theoretical limits of microalgal H<sub>2</sub> production systems, emerging strategies to engineer next-generation systems and how these fit into an evolving H<sub>2</sub> economy.

**Keywords:** algae, solar, hydrogen, water, renewable energy, fuel.

## Introduction

The global economy is valued at ~US\$100 Tn pa (CIA, 2014) and is powered by the \$6 Tn pa energy sector (Dittrick and Izundu, 2008), with ~80% provided in the form of fuel and ~20% as electricity (IEA, 2009). While renewable electricity generation systems are being deployed rapidly, renewable fuel technologies are ~10–20 years behind on the development curve. This is due to the challenges of reducing fuel production costs towards ~\$100 per barrel of oil equivalent to compete with fossil fuels, and the need to improve 'Energy Return on Energy Invested' (EROEI – a measure of process efficiency) and reduce greenhouse gas (GHG) emissions.

Additionally, by 2050 the human population is forecast to increase from 7.3 billion to over 9 billion people (USCB, 2013), and together with continued global economic growth, this is projected to require 50% more fuel (IEA, 2010), 70% more food (FAO, 2009), 50% more fresh water (OECD, 2014) and cuts in CO<sub>2</sub> emissions of 80% (IPCC, 2007; Stocker, 2013) to maintain political, social, fuel and climate security. It is therefore critical to fast-track the development of 'commercially-ready' CO<sub>2</sub> neutral fuel systems that do not compete with food and water needs. The importance of this challenge is highlighted by the common vision of the Group of 7 (G7) nations to achieve GHG reductions of 70% by 2050 based on 2010 figures (G7, 2015).

## Solar fuel options

The production of clean fuels at a globally significant level requires a renewable energy source sufficiently large to drive this process. Solar energy is by far the largest energy source available to us, with 5500 ZJ (1 ZJ = 10<sup>15</sup> J) (Smil, 2008) reaching the Earth's atmosphere every year. Of this, 1300 ZJ is photosynthetically active radiation (PAR) available at the Earth's surface (Oey *et al.*, 2013). This annual irradiance level (1300 ZJ/year) is ~2300× the total global energy demand (0.56 ZJ/year) (BP, 2011) and dwarfs the combined energy from all reported oil, coal, gas and uranium reserves (Stephens *et al.*, 2010b). Photosynthetic organisms have over 3 billion years, evolved intricate photosynthetic systems capable of tapping into this abundant solar resource for the production of food, fuel and atmospheric oxygen (O<sub>2</sub>) and not only support life on Earth, but provide a basis for next-generation solar fuel production.

First and second generation crop-based biofuels include sugar and corn ethanol, as well as lignocellulosic ethanol from woody biomass and agricultural residues. However, these technologies require arable land and fresh water, and so ultimately result in 'food vs fuel' or 'forest vs fuel' competition (e.g. palm oil). To achieve a transition from 'food/forest vs fuel' scenarios to a 'food and fuel' future, next-generation biofuel systems will need to expand photosynthetic capacity into urban areas, onto nonarable land (~25% of the Earth's surface), or into the oceans to utilize

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alternative water sources and conserve arable land (~3% of the Earth's surface) (Stephens *et al.*, 2012). Microalgae and cyanobacteria systems can be located on nonarable land (and potentially in urban areas and oceans), cultivated at least in part in saline and/or waste water, facilitating increased nutrient and water recycling, and achieve higher yields than crop plants due to the ability to optimize light distribution, CO<sub>2</sub> supply and production conditions and thus offer advantages over crop-based biofuel feed stocks (Pulz and Gross, 2004).

It can be calculated that at a 2% solar to biomass conversion efficiency, which is already achievable at demonstration scale for biomass production in microalgal systems, ~2.15% of the Earth's surface would be required to supply the current global energy demand in the form of biomass at average illumination levels ( $0.56 \text{ ZJ/year}/1300 \text{ ZJ/year} \times 100/2 = 2.15\%$ ). Subsequent production of fuels (e.g. oil, bio-diesel, ethanol, methane and H<sub>2</sub>) reduces this efficiency, but this is offset, at least in part, by the fact that natural photosynthesis can attain theoretical efficiencies of ~6% (Melis and Happe, 2001; Zhu *et al.*, 2008, 2010). Engineered microalgae and artificial systems, particularly those capable of H<sub>2</sub> production, can theoretically achieve higher efficiencies, but require further development (Blankenship *et al.*, 2011; Kruse *et al.*, 2005b; Melis, 2009). This article reviews advances in the development of microalgae-based solar-driven H<sub>2</sub> production processes from water, with a particular focus on the challenges that must be overcome to deliver them and potential solutions that they offer.

## Microalgal H<sub>2</sub> production

The increasing requirement for carbon emission reduction makes H<sub>2</sub> more attractive as a fuel as its combustion yields only H<sub>2</sub>O. Furthermore, H<sub>2</sub> has a 2.7–3.09 higher energy density (~120 (LHV) – 140 (HHV) kJ/g) than other hydrocarbon fuels (Gupta *et al.*, 2013). Conventional, fossil fuel-based H<sub>2</sub> production methods (e.g. steam reformation of natural gas (50%), industrial oil and naphtha reforming (30%), coal gasification (18%) and fossil fuel driven water electrolysis (3.9%) (Gupta *et al.*, 2013; Kalamaras and Efsthathiou, 2013)) are costly, energy intensive and emit high levels of CO<sub>2</sub>. In comparison, renewable bio-H<sub>2</sub> production systems (such as microalgae and cyanobacteria systems) have the potential to be carbon negative and less energy intensive, as they operate at ambient temperature and pressure (Karthic and Joseph, 2012).

Hydrogen production using oxygen evolving photosynthesis (oxygenic photosynthesis) is the most advanced biological H<sub>2</sub> production approach and the focus of this article. It uses solar energy to split water into protons (H<sup>+</sup>), electrons (e<sup>-</sup>) and O<sub>2</sub> (Figure 1a) and recombines the derived H<sup>+</sup> and e<sup>-</sup> by either hydrogenase (Figure 1b) or nitrogenase enzymes to produce H<sub>2</sub>. The utilization of H<sup>+</sup> and e<sup>-</sup> derived from water photolysis for H<sub>2</sub> production has only been reported in green algae and cyanobacteria, and provides the basis for the development of bio-inspired artificial photosynthetic systems (Blankenship *et al.*, 2011). The water photolysis process can be divided into indirect and direct pathways.

### Indirect water photolysis H<sub>2</sub> production process

The indirect process can take place in both microalgae and cyanobacteria (Kruse *et al.*, 2005a; Mathews and Wang, 2009; Melis and Happe, 2001; Melis *et al.*, 2000; Rathore and Singh, 2013). Solar energy is first converted into chemical energy in the form of carbohydrates, which are then used as substrates for H<sub>2</sub> production. Cyanobacteria, depending on the species, utilize

both nitrogenases and hydrogenases for H<sub>2</sub> production (Dutta *et al.*, 2005), whereas microalgae rely solely on hydrogenases (Oncel *et al.*, 2015). Nitrogenases have the advantage that they act unidirectionally, whereas hydrogenases are bidirectional (Melnicki *et al.*, 2012). However, the high O<sub>2</sub> sensitivity of both enzymes requires the separation of H<sub>2</sub> evolution and CO<sub>2</sub> fixation. In cyanobacteria, the reactions are either temporally separated during light and dark periods, or physically separated, with H<sub>2</sub> production occurring in heterocysts and CO<sub>2</sub> fixation in the vegetative cells (Dutta *et al.*, 2005). The low ratio of heterocysts to vegetative cells (about 1:10) limits H<sub>2</sub> production levels (Bandyopadhyay *et al.*, 2010). High H<sub>2</sub> production rates have been reported using cyanobacteria as catalysts (i.e. through the inhibition of cell replication) (Bandyopadhyay *et al.*, 2010; Melnicki *et al.*, 2012). However, the energy requirement for the nitrogenase reaction (4 ATP per H<sub>2</sub>) reduces H<sub>2</sub> production and conversion efficiencies to less than half of the efficiencies expected from hydrogenase-based indirect photolysis (LaurentPilon and Halil, 2014). In algal systems, the most common, but not ideal practice, is the temporal separation of the O<sub>2</sub> and H<sub>2</sub> production phase (aerobic and anaerobic phase, Figure 1) to circumvent oxygenic inactivation of the hydrogenase (further described below) (Kruse *et al.*, 2005a; Melis and Happe, 2001; Melis *et al.*, 2000).

### Direct water photolysis H<sub>2</sub> production process

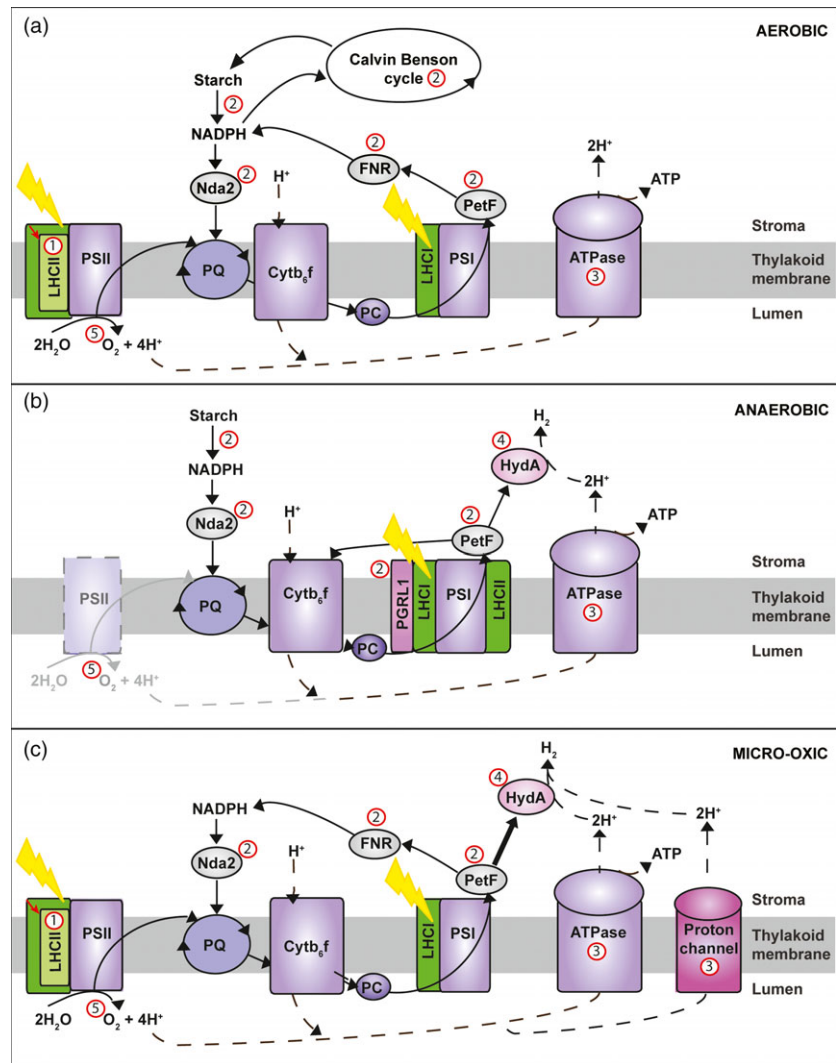
Direct photolysis has only been reported in microalgae, and involves the funnelling of e<sup>-</sup> derived from the light-driven water splitting reaction of photosystem II (Figure 1c) directly to a H<sub>2</sub>-producing hydrogenase (Melis and Happe, 2001; Melis *et al.*, 2000). While direct solar-driven H<sub>2</sub> production from water offers the highest theoretical photon conversion efficiency, achieving this is technically challenging due to the high O<sub>2</sub> sensitivity of the hydrogenase. It requires customized cell lines and production systems which allow the simultaneous production of H<sub>2</sub> and O<sub>2</sub> as this co-production is tightly down-regulated in native strains (Melis *et al.*, 2000).

To date, the highest bio-H<sub>2</sub> production efficiencies have been reported for microalgae (Scoma *et al.*, 2012; Volgusheva *et al.*, 2013). In microalgae, the first step of photosynthesis is the capture of solar energy by the light-harvesting complex (LHC) proteins (Figure 1a). The LHC proteins are classified as LHCI or LHCII types depending on their predominant interaction with either photosystem I (PSI) or II (PSII), respectively. The LHC proteins belong to a large gene family, which in the green alga, *Chlamydomonas reinhardtii*, consists of over 20 members (Dittami *et al.*, 2010). The excitation energy transferred to PSII by LHCII (Figure 1a) drives the photosynthetic water splitting reaction which converts H<sub>2</sub>O into H<sup>+</sup>, e<sup>-</sup> and O<sub>2</sub> (Eq. 1).

The photons captured by LHCI and LHCII excite e<sup>-</sup> derived from H<sub>2</sub>O, and drive their transfer along the photosynthetic electron transport chain (e<sup>-</sup> flow is indicated by solid black lines in Figure 1a) from the PSII-LHCII supercomplex via plastoquinone (PQ), cytochrome b<sub>6</sub>f (Cyt), the PSI-LHCI supercomplex and ferredoxin (Fd) (via the ferredoxin-NADP<sup>+</sup> oxido-reductase; FNR) to finally reduce NADP<sup>+</sup> to NADPH. NADPH, together with ATP, is used in the Calvin-Benson cycle and subsequent biochemical pathways to fix (i.e. reduce) CO<sub>2</sub> to the sugars, starch, oils and other bio-molecules which collectively form biomass.

Simultaneously, H<sup>+</sup> are released into the thylakoid lumen by PSII and the PQ/PQH<sub>2</sub> cycle (H<sup>+</sup> flow is indicated by black dashed lines in Figure 1). These H<sup>+</sup> generate an electrochemical H<sup>+</sup>

**Fig. 1** Overview of the photosynthetic microalgal H<sub>2</sub> production from water. Aerobic (a) and anaerobic (b) stages of the two phase H<sub>2</sub> production and Micro-oxic continuous H<sub>2</sub> production (c). Proton (H<sup>+</sup>) flow is marked with dashed lines, electron flow with continuous lines. Potential engineering targets for improved H<sub>2</sub>-production are marked in red (labels #1–5) and described in detail in section ‘Biological challenges and bottlenecks for microalgal H<sub>2</sub>-production’. LHCII: light-harvesting antenna proteins of photosystem II; PSII: photosystem II reaction centre; PQ: plastoquinone pool; Cytb<sub>6</sub>f: cytochrome b<sub>6</sub>f complex; PC: plastocyanin; PGRL1: proton gradient regulation like1 protein; LHCI: light-harvesting antenna proteins of photosystem I; HydA: hydrogenase A; PETF: ferredoxin; FNR: ferredoxin (flavodoxin)-NADP(H) reductase; NDH: NADPH-dehydrogenase.



gradient across the thylakoid membrane, which drives ATP production via the flow of H<sup>+</sup> back to the stroma through the ATP synthase.

Under normal aerobic conditions (Figure 1a), photosynthesis produces the carbohydrates that fuel mitochondrial respiration and cell growth. However, under anaerobic light conditions (Figure 1b), mitochondrial oxidative phosphorylation is largely inhibited by the lack of oxygen, leading to chloroplast over-reduction and a slowing of the electron transport chain, which can ultimately result in photo-damage and reduced ATP generation. Under these conditions, the H<sup>+</sup> and e<sup>-</sup> extracted from water by the remaining PSII or starch can be fed to the hydrogenase (HYDA) via the electron transport chain, which recombines the H<sup>+</sup> and e<sup>-</sup> to produce H<sub>2</sub> (Eq. 2).

Overall therefore, Eqs 1 and 2 describe solar-driven H<sub>2</sub> production from H<sub>2</sub>O. The hydrogenase essentially acts as a H<sup>+</sup>/e<sup>-</sup> release valve by recombining H<sup>+</sup> (from the medium) and e<sup>-</sup> (from reduced ferredoxin) to produce H<sub>2</sub> gas that is excreted from the cell.



and



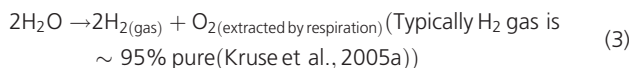
The high H<sub>2</sub> production efficiency of microalgae is partly due to the high efficiency of the algal [FeFe]-hydrogenase, which is 100-fold higher than that of other hydrogenases (turnover rate of up to 10<sup>4</sup> H<sub>2</sub> molecules/s) (Lubitz *et al.*, 2014; Volgusheva *et al.*, 2013, 2015). The overall process is also attractive for sustainable applications as it occurs at ambient temperature and pressure. The volatility of H<sub>2</sub> has the advantage that it prevents feedback inhibition and its separation into the gas phase assists harvesting, although there are technical challenges in terms of H<sub>2</sub> containment and its separation from contaminating oxygen.

*Chlamydomonas reinhardtii* is one of the best studied microalgal species with respect to H<sub>2</sub> production processes, availability of genetic tools and structural biology knowledge of the photosynthetic machinery (Nield *et al.*, 2004; Posten and Walter, 2012; Tokutsu *et al.*, 2012). It is not only able to produce H<sub>2</sub> via oxygenic photolysis (direct and indirect), but also via dark fermentation (see below), in a process similar to that of other micro-organisms (Eroglu and Melis, 2011; Stripp and Happe, 2009; Tolleter *et al.*, 2011; Volgusheva *et al.*, 2013; Wecker and Ghirardi, 2014). Of these pathways, light-dependent H<sub>2</sub> production is the most direct photon-to-fuel conversion process. However, the natural hydrogenase is only expressed and active under micro-oxic or anaerobic conditions (Ghirardi *et al.*, 1997) and is rapidly inactivated by the gradual accumulation of

photosynthetically produced  $O_2$ . While this provides the basis for a ~95% pure  $H_2$  stream (Kruse et al., 2005a) and potentially protects against the formation of explosive  $O_2/H_2$  mixtures, under natural conditions it only allows for transient  $H_2$  production.

Currently, most algal systems are based on a simple process of temporal separation to circumvent the oxygenic inactivation of the hydrogenase (Melis et al., 2000). This involves first growing algae aerobically for biomass accumulation, ideally by  $CO_2$  fixation, during which oxygen is released and the reducing power stored, typically as carbohydrates (Figure 1a). This step is followed by sulphur (S) starvation. Among other changes, S deprivation reduces the rate of repair of a PSII reaction centre protein (D1), which contains the S-containing amino acid methionine. Photo-damage then reduces PSII to ~25% of the original level (Volgusheva et al., 2013). This drops the  $O_2$  production below the rate of mitochondrial respiration and achieves the anaerobic/micro-oxic conditions which induce the expression of an active hydrogenase (Figure 1b). While anaerobiosis initially blocks the  $e^-$  transport from the remaining PSII in the phase preceding  $H_2$  production, the block is subsequently released and direct  $e^-$  transport to the hydrogenase occurs, with ~80% of the  $H_2$  being derived directly from PSII activity (Volgusheva et al., 2013). Under these conditions, the reactions described in Eqs 1 and 2 are effectively coupled, resulting in the overall process described in Eq. 3. However, they also limit the overall efficiency of the process.

To overcome the limitations of S deprivation, other approaches aim to develop  $O_2$ -tolerant hydrogenases or balance  $O_2$  production with metabolic  $O_2$  utilization (Oey et al., 2013). A further approach is the use of S microdosing (Figure 1c) (Kosourov et al., 2005) to allow PSII repair, the production of  $H^+$  and  $e^-$  from water and to balance  $O_2$  evolution with  $O_2$  utilization through mitochondrial respiration (Kruse et al., 2005a). This micro-oxic approach has the advantage of being more efficient and can provide a basis for a continuous  $H_2$  production process. Another, recently published strategy is magnesium deprivation, which results in a decreased photosynthetic activity but increased respiration and starch accumulation allowing a prolonged  $H_2$  production period (>7 days). Under these conditions, functional PSII, which appears to be crucial for  $H_2$  production, was only reduced by 20%, implying a higher  $e^-$  availability to the hydrogenase (Volgusheva et al., 2015). Furthermore, the co-cultivation of algae and bacteria has been presented as a new approach to achieve algal anaerobiosis via increased bacterial respiration (Lakatos et al., 2014). It is also of note that two algae strains are reported to be able to produce low levels of  $H_2$  under aerobic conditions (Hwang et al., 2014).



## Biological challenges and bottlenecks for microalgal $H_2$ production

In addition to *Chlamydomonas*, several other algal species, including species of *Chlorella* (Rashid et al., 2011), *Scenedesmus* (Schulz et al., 1998) and *Tetraselmis* (D'Adamo et al., 2014), have also been reported to produce  $H_2$  but at lower levels. The *C. reinhardtii* system has the advantage that all three genomes (nuclear, chloroplast and mitochondrial) have been sequenced

and transformed, and much more detailed information is available on the organization of photosynthetic complexes during  $H_2$  production (Hemschemeier and Happe, 2011; Tolleter et al., 2011). Transformation techniques are well established and include particle bombardment (Debuchy et al., 1989; Kindle et al., 1989; Mayfield and Kindle, 1990), glass bead or silicon-carbide whisker methods (Dunahay, 1993; Kindle, 1990), electroporation (Shimogawara et al., 1998) and *Agrobacterium tumefaciens*-mediated gene transfer (Kumar et al., 2004). *Chlamydomonas* therefore remains the best characterized model organism for microalgal  $H_2$  production, associated genetic engineering and the identification of molecular bottlenecks.

## Optimizing light capture efficiency

The LHC antennae systems have a dual role: to capture photons and dissipate excess light energy to provide photoprotection (Niyogi, 1999; Pascal et al., 2005; Takahashi et al., 2006). Biomass production efficiency, at least in the laboratory, can be improved through LHC antenna reduction (Figure 1 – label #1), as this enhances light distribution through the bioreactors, enables the use of increased operational cell concentrations and can yield improved overall photosynthetic efficiencies of these systems (Beckmann et al., 2009; Melis et al., 1999; Mussgnug et al., 2007; Oey et al., 2013; Polle et al., 2003). Furthermore, *C. reinhardtii* antenna mutants have also been reported to exhibit an earlier onset of  $H_2$  production under S deprivation conditions (Oey et al., 2013), which is likely due to three factors: (i) improved light distribution leading to higher photon conversion efficiencies of the overall culture, (ii) the ability to lower the dissolved  $O_2$  concentration through the use of higher cell densities, which balance  $O_2$  production with metabolic load, and (iii) altered photo-inhibition and stabilization of PSII required for subsequent  $H_2$  production (Volgusheva et al., 2013). Collectively these properties resulted in cultures exhibiting higher  $H_2$  production rates under the conditions tested (Oey et al., 2013).

The precise engineering of the LHC antenna requires a detailed understanding of the structural complexity and dynamic response of algae to light in larger scale production systems (de Mooij et al., 2015). To date, the engineering of the nuclear encoded antenna genes has utilized chemical or random insertion mutagenesis (Polle et al., 2002, 2003), the manipulation of antenna regulation proteins (e.g. NAB1 (Beckmann et al., 2009)) or RNAi knock-down approaches (Mussgnug et al., 2007; Oey et al., 2013).

The least specific method of engineering antenna mutants involves the introduction of foreign DNA into the nuclear genome via *random insertion* (Zhang et al., 2014). As clear phenotypes are needed for the rapid screening of mutants, the expected light green phenotypes of putative antenna mutants seems an attractive selection criteria. However, while this approach identifies mutants impaired in antenna or chlorophyll synthesis, it does not select for specific multiple mutations likely required for optimal  $H_2$  production.

A more targeted approach to engineer antenna cell lines is via the indirect route of manipulating antenna regulation proteins. An example of this is the over-expression of the translational repressor NAB1, which results in the specific down-regulation of specific LHC proteins (Beckmann et al., 2009). This approach relies on cellular regulatory mechanisms and is therefore limited in its target scope. Another approach is RNAi mediated knock-down (De Riso et al., 2009; Moellering and Benning, 2010; Molnar et al., 2007, 2009; Rohr et al., 2004; Schmollinger et al., 2010;



Sun *et al.*, 2008; Zhao *et al.*, 2007, 2009) of specific target genes such as *LHC* genes, or genes involved in chlorophyll biosynthesis. A challenge for precise antenna engineering is that the coding regions of the *LHC* genes are highly homologous (Natali and Croce, 2015), which complicates the specific down-regulation of target *LHC* genes. Additionally, the need to maintain the *RNAi* expressing mutants, typically through ongoing selective pressure, makes this approach less than ideal for industrial scale up. *RNAi* is therefore best suited for proof-of-principle studies to identify target genes.

The most elegant technologies facilitate precise and permanent genome editing enabling the fine tuning of antenna genes and adjustments to the pigment content, expanding the available solar spectrum (Blankenship and Chen, 2013; Chen and Blankenship, 2011). Several genome editing systems have been developed in recent years, including zinc finger nucleases (ZFN) (Sizova *et al.*, 2013), transcription activator-like effector nucleases (TALENs) (Gao *et al.*, 2014) and the CRISPR/Cas systems (Cho *et al.*, 2013; Mali *et al.*, 2013), all of which rely on nuclease-induced DNA strand breaks and endogenous cell repair mechanisms to obtain mutants with specifically edited genomes. This allows processes such as photosynthesis to be fine-tuned for biotechnological applications. Another attraction of these techniques is the potential to develop mutants which are nongenetically modified organisms due to the transient introduction of the required nucleases. This would be a significant advance for large-scale applications such as biofuel production, particularly given current legislative limitations on the use of GMO strains.

While ZFN (Sizova *et al.*, 2013) and TALENs (Gao *et al.*, 2014) have been used for genome editing in *Chlamydomonas*, they still involve labour-intensive cloning steps. In contrast, the CRISPR/Cas system (Cho *et al.*, 2013; Mali *et al.*, 2013) promises to be a simpler technique only requiring the expression of an RNA guided nuclease, Cas9, to introduce strand breaks. The template for the guide RNA is fairly short (~23 bp), assisting with the targeted engineering of specific antenna genes given their high level of homology. Although successful CRISPR/Cas usage in *Chlamydomonas* is yet to be reported, it is anticipated that this technique will be possible in *Chlamydomonas* in the near future (Jiang *et al.*, 2014), having already been successfully demonstrated in mammalian cells (Cong *et al.*, 2013; Mali *et al.*, 2013; Park *et al.*, 2014), plants (Fauser *et al.*, 2014; Feng *et al.*, 2013; Xie and Yang, 2013) and zebra fish (Hwang *et al.*, 2013). A patent application for its usage in the algal genus *Nannochloropsis* is also encouraging (Patent US 20140220638 A1).

### Electron supply to the hydrogenase and availability of reduced PETF

Limited electron flow to the hydrogenase is another potential bottleneck for sustainable H<sub>2</sub> production (Hallenbeck and Benemann, 2002) (Figure 1 – label #2). This can occur due to the limited availability of reduced ferredoxin (PETF) as a result of other competing pathways (Winkler *et al.*, 2011) (e.g. ferredoxin-NADP<sup>+</sup> reductase (FNR), sulphite reductase, nitrate reductase, glutamate synthase and fatty acid desaturases (reviewed in Hemschemeier and Happe, 2011)). The hydrogenase (HYDA) can accept e<sup>-</sup> via a direct (PSII-dependent; 2 photons per electron to HYDA) or indirect (PSII-independent from starch; 3 photons per electron to HYDA) route (Chochois *et al.*, 2009; Fouchard *et al.*, 2005). To improve electron flow, PETF, FNR and the hydrogenase have all been engineered (Long *et al.*, 2009; Lubner *et al.*, 2011; Rumpel *et al.*, 2014; Sun *et al.*, 2013; Wittenberg *et al.*, 2013;

Yacoby *et al.*, 2011), with a particular focus on the improvement of the affinity of the hydrogenase to PETF, the reduction of the affinity of PETF for FNR and the fusion of PETF and PSI with the hydrogenase. However, the identified candidates have so far only been tested *in vitro* and are yet to be assessed for their performance *in vivo*. Photosynthetic, H<sub>2</sub> producing algal cells supply an excellent scaffold to carry out such proof of principle studies. While most engineering efforts have focused on the chloroplast-localized nuclear encoded genes, recent efforts have been made towards the *in situ* overexpression of the hydrogenase in the plastid to uncouple it from its native control system (Reifschneider-Wegner *et al.*, 2014). Engineering has also focused on indirect targets, including electron competitors such as RuBisCo (Pinto *et al.*, 2013), cyclic electron flow (Kruse *et al.*, 2005a; Tolleter *et al.*, 2011), starch degradation (Chochois *et al.*, 2009) and respiration (Ruehle *et al.*, 2008), with mutants in all of these pathways reportedly yielding increased H<sub>2</sub> production levels. Finally, additional components have been added to the electron transfer pathway, including a plastid-expressed NAD(P)H dehydrogenase (Baltz *et al.*, 2014), a hexose transporter (Doebbe *et al.*, 2007) and exogenous hydrogenases (Chien *et al.*, 2012).

### Alteration of the thylakoid proton gradient

Proton supply to the hydrogenase is another potential bottleneck (Figure 1 – label #3). The transport of e<sup>-</sup> from water to PETF via the photosynthetic electron transport chain is involved in establishing a proton gradient across the thylakoid membrane which drives ATP synthesis. While ATP production is essential during CO<sub>2</sub> fixation, the ATP requirement drops during H<sub>2</sub> production (Das *et al.*, 2014) and electron transport is reduced at the point of *Cytb<sub>6</sub>f* (Antal *et al.*, 2009; Burgess *et al.*, 2011), leading to an impaired dissipation of the proton gradient and therefore decreased proton availability for the hydrogenase and reduced H<sub>2</sub> production. One strategy to improve H<sub>2</sub> production is to artificially dissipate the proton gradient to increase H<sub>2</sub> production transiently in the presence of the chemical uncoupler carbonyl cyanide *m*-chlorophenyl hydrazine (CCCP), which causes an efflux of H<sup>+</sup> from the thylakoid lumen into the stroma (Kruse *et al.*, 2005a; Lee, 2013; Lee and Greenbaum, 2003). This suggests that the integration of a proton channel into the thylakoid membrane could more permanently restore proton and electron flow to the hydrogenase. Such a proton channel, however, would need to be inducibly expressed, as the addition of the uncoupler prior to anaerobiosis was found to abolish hydrogenase activity, suggesting that the proton gradient is important for initial hydrogenase expression (Lee, 2013) and aerobic growth. A similar strategy involves the development of a leaky ATPase to increase proton flow and reduce ATP production (Das *et al.*, 2014; Robertson *et al.*, 1990). Reduced ATP production caused by the introduction of a proton channel or mutated ATPase may additionally reduce reactions competing for reducing equivalents and therefore increase electron supply to the hydrogenase (Kumar and Das, 2013).

### Oxygen sensitivity of the hydrogenase

Sustained H<sub>2</sub> production under standard growth conditions remains a major challenge, as O<sub>2</sub> sensitivity of the hydrogenase is a multifaceted problem. This is because O<sub>2</sub> oxygen inhibits not just hydrogenase enzyme function, but also transcription and protein maturation (Cohen *et al.*, 2005). Interestingly, two algae strains were recently reported to be able to express the hydrogenase in the presence of more than 21% O<sub>2</sub> and to

produce low levels of H<sub>2</sub> at 15% atmospheric O<sub>2</sub> (Hwang *et al.*, 2014). Several genetic engineering approaches have also been tested to reduce the O<sub>2</sub> sensitivity of the hydrogenase (Figure 1 – label #4), including random mutagenesis (Flynn *et al.*, 2002) and targeted mutagenesis of the catalytic site to restrict O<sub>2</sub> access (Stiebritz and Reiher, 2012). While engineering approaches have been successful for a bacterial [NiFe] hydrogenase (Dementin *et al.*, 2009), this has so far not been the case with the microalgal [FeFe] hydrogenase. Despite this, the identification of hydrogenases with reduced O<sub>2</sub> sensitivities will increase the scope for genetic engineering. A hydrogenase with a reduced O<sub>2</sub> sensitivity would open up a direct path to H<sub>2</sub> production from oxygenic water splitting, but would also lead to the co-production of O<sub>2</sub>, which then requires subsequent gas separation. However, this approach would overcome the need for a two phase aerobic/anaerobic process, potentially enabling a continuous H<sub>2</sub> production process and eliminating the need for ATP and NADPH, which are required to produce starch- and oil-based feed stocks for alternative fuels. Achieving this in thermophiles would be expected to further improve reaction kinetics.

### Oxygen evolution and removal

A different approach used to alter O<sub>2</sub> sensitivity and extend H<sub>2</sub> production is to control the O<sub>2</sub> concentration of the culture. Increasing the cell density and respiratory load can result in an earlier onset of anaerobiosis and H<sub>2</sub> production (Oey *et al.*, 2013; Schönfeld *et al.*, 2004). Furthermore, the down-regulation of PSII (Surzycki *et al.*, 2007) and engineering of O<sub>2</sub> evolution activity (Makarova *et al.*, 2007; Scoma *et al.*, 2012; Torzillo *et al.*, 2009) have been exploited (Figure 1 – label #5). Leghemoglobins, which are able to sequester O<sub>2</sub>, have also been expressed in *C. reinhardtii* (Wu *et al.*, 2010, 2011), and in a different approach, a sulphate permease mutant was developed, which allowed greater control of S deprivation (Chen *et al.*, 2005).

### H<sub>2</sub>-production improvement strategies - Supportive targets

Despite the obvious benefit of manipulating targets directly involved in H<sub>2</sub> production, engineering more indirect targets to simplify cultivation, analysis and H<sub>2</sub> production is also important. The ability to easily report lumen pH (Bencina, 2013; Demareux, 2002), hydrogenase expression and key metabolic pathways such as sulphur, starch and lipid metabolism, combined with external control of gene expression levels and physiological mechanisms via the supply of stimuli such as hormones or light, would enable the rapid dissection of the changes in cell state occurring during H<sub>2</sub> production. New genome editing tools (Cong *et al.*, 2013; Fauser *et al.*, 2014; Feng *et al.*, 2013; Hwang *et al.*, 2013; Mali *et al.*, 2013; Park *et al.*, 2014; Xie and Yang, 2013) will provide scope for sophisticated gene regulation and diagnosis similar to those used in mammalian systems including inducible promoters and self-altering genes (Cre-lox (floxed) systems) (Hajdukiewicz *et al.*, 2001; Oey *et al.*, 2009), highly specific reporter systems and further tools for improving research and industrial use.

### High-throughput screening methods

The development of new H<sub>2</sub> screening methods can also accelerate the engineering of enhanced H<sub>2</sub>-producing algal strains. To date, H<sub>2</sub> mutants have been detected through a chemo-chromic sensing assay, which utilizes a palladium/tungsten oxide film (Seibert *et al.*, 1998) or in screens specific to the created mutants (Kruse *et al.*, 2005a; Ruehle *et al.*, 2008;

Stapleton and Swartz, 2010; Tolleter *et al.*, 2011). A recent H<sub>2</sub>-detection screen developed (Wecker and Ghirardi, 2014), which uses *Rhodobacter capsulatus* expressing an emerald green fluorescent protein (emGFP) driven by the *hupR* H<sub>2</sub>-sensing promoter as a reporter for H<sub>2</sub> production, offers a simple, inexpensive and semi-quantitative screening method. The development of a chlorophyll fluorescence assay (Godaux *et al.*, 2013) and an inorganic hydrogenase active site mimic will also allow for quicker screening of hydrogenase mutants (Berggren *et al.*, 2013; Esselborn *et al.*, 2013).

## Microalgae: a blueprint and evaluation platform for bio-inspired hydrogen production

Natural microalgae-based light-driven H<sub>2</sub> production processes serve as a blueprint and testing platform for the development of bio-inspired artificial solar H<sub>2</sub> production systems. For example, at the level of component development, the atomic structure of the light-harvesting antenna systems provides valuable insights into the design of engineered and artificial light capturing pigments and systems (Qin *et al.*, 2015). Another example is the design of new water splitting catalysts based on the manganese cluster of PSII (Brimblecombe *et al.*, 2010; Tsui *et al.*, 2013; Zhang *et al.*, 2015). The arrangement of the redox-active components of the photosystems has also been studied extensively, and other research has led to the development of self-assembling synthetic scaffolds able to optimize the coordination and spacing of the components of artificial photosynthetic systems (Farid *et al.*, 2013; Mancini *et al.*, 2013; Weingarten *et al.*, 2014). In this context, it is notable that the hydrogenase of *C. reinhardtii* can be prepared in large quantities as an apo-protein and be readily reconstituted with its iron sulphur clusters to form an active hydrogenase (Esselborn *et al.*, 2013). Through the use of such components, it is therefore theoretically possible to build light-driven redox-active systems which split water and use the H<sup>+</sup> and e<sup>-</sup> for H<sub>2</sub> production. However, the economic viability and EROEI of both algae and bio-inspired artificial systems will have to be determined later in the development cycle.

## Challenges of scale up

### Coordinated biological engineering

The selection and engineering of high-efficiency microalgae cell lines is central to this process. Lessons learnt from the optimization of microalgal H<sub>2</sub> production suggest that the highest efficiency strains will require not single mutations, but significant re-engineering of the H<sub>2</sub> production process. For example, down-regulating the light-harvesting proteins has benefits as light green cell lines enable higher cell densities to be used, resulting in more rapid O<sub>2</sub> scavenging, the early onset of H<sub>2</sub> production and an overall higher H<sub>2</sub> yield (Oey *et al.*, 2013). The yield of H<sub>2</sub> can also be increased by locking the photosynthetic electron transport chain into the State 2 configuration and by reducing cyclic electron transport, which competes with the hydrogenase for e<sup>-</sup> (Kruse *et al.*, 2005a; Tolleter *et al.*, 2011). Additionally, lessening the competition between the hydrogenase and FNR for electrons for example, by re-engineering the electron donors of the hydrogenase could further improve H<sub>2</sub> production (Rumpel *et al.*, 2014). The ultimate goal would be the combination of all of these targeted mutations into a single production strain for continuous H<sub>2</sub> production. It would essentially allow the microalgae cells to act as catalysts under micro-oxic conditions where O<sub>2</sub> production

and consumption are in balance (Figure 1c), and the water splitting reaction is active at the same time as the hydrogenase. This would enable a 2 photon vs 3 photon electron transfer steps from water to H<sub>2</sub>, which represents a 33% improvement in process efficiency.

### Next-generation photobioreactor development

The scale up of microalgae systems from the laboratory to commercial facilities theoretically offers the potential to couple H<sub>2</sub> fuel production to CO<sub>2</sub> sequestration (e.g. the residual biomass to biochar) or other co-products. To establish the viability of a given process, rigorous techno-economic (TEA) and life cycle analyses (LCA), as well as pilot and demonstration scale trials, are required to confirm positive economic returns and ERoEI, as well as reduced GHG emissions. Achieving these targets will not only involve the engineering of next-generation cell lines as described above, but the design of photobioreactors able to deliver optimized production conditions for the chosen production strains and specific geographic locations (Franz *et al.*, 2012; Slegers, 2014; Slegers *et al.*, 2011).

### Other artificial and naturally derived renewable H<sub>2</sub>-production strategies

To replace fossil fuel-based H<sub>2</sub> production processes, several renewable H<sub>2</sub> production strategies are being explored. In addition to biological systems such as algae, these include biologically based or biologically inspired systems as well as physical systems such as PV, wind and wave power. The ability to use electrolysis at peak electricity production times to generate H<sub>2</sub> for energy storage is already being employed by current European demonstration projects such as HyUnder, INGRID, MYRTE and GRHYD (AREVA, 2013; D'Errico and Screnci, 2012; Darras *et al.*, 2012; ENGIE; HyUnder, 2012; INGRID; Poggi *et al.*, 2014). Coupling such energy capture and electrolysis processes is more environmentally friendly than using fossil fuels, and could technically provide workable solutions which can reportedly achieve photon-to-electron conversion efficiencies of 20% (Bonke *et al.*, 2015). Nevertheless, challenges to the scale up of these technologies remain. These include the following: (i) driving down the capital costs of production, (ii) eliminating rare earth metals (Kapdan and Kargi, 2006), (iii) increasing the catalyst longevity and (iv) improving the ERoEI towards a value of 10:1 required to support a civilized society (Hall *et al.*, 2009).

Microalgae systems currently only have photon conversion efficiencies of 3% (Scoma *et al.*, 2012; Volgusheva *et al.*, 2013) and a theoretical maximum of ~12–14% (Melis, 2009; calculated based on the Z-scheme of electron transport and mean energy of PAR), which is lower than that of artificial systems (Bonke *et al.*, 2015). However, they are self-replicating and repairing, have water splitting complexes and hydrogenases based on manganese, calcium and iron (not rare Earth metals) and have been proven to be able to support H<sub>2</sub> production over long periods (Laurinavichene *et al.*, 2006). Furthermore, H<sub>2</sub>-producing microalgae can be used in co-production strategies which theoretically have the potential to improve economic performance (Stephens *et al.*, 2010a). More detailed TEA and LCA are required to establish the pros and cons of each technology and which system is more competitive economically in terms of ERoEI and GHG emissions.

Biological H<sub>2</sub> production can, apart from the above discussed oxygenic photosynthesis, further be achieved via microbial

electrolysis cells, dark fermentation and photo-fermentation (nonoxygenic photosynthesis) (Chandrasekhar *et al.*, 2015).

### Microbial electrolysis cells

are designed to produce H<sub>2</sub> from electrogenic micro-organisms which consume and release e<sup>-</sup>, H<sup>+</sup> and CO<sub>2</sub>. An externally supplied voltage allows the formation of H<sub>2</sub> gas from the released H<sup>+</sup>. As the H<sub>2</sub> production process itself does not occur inside the cell, microbial electrolysis cells are strictly speaking not bio-H<sub>2</sub> production platforms. Additionally, due to the requirement of the external supply of an electric current and carbon-based feed stocks, the economic viability of scaling up this H<sub>2</sub> production strategy must be carefully considered (Heidrich *et al.*, 2014).

### Dark fermentation

involves the production of H<sub>2</sub> using facultative or obligate anaerobic bacteria which also consume organic material. However, this is a chemical energy conversion process rather than a renewable energy process. Furthermore, while the process occurs at a higher rate compared to photo-fermentation or photolysis, it has a low H<sub>2</sub> yield: substrate use ratio, mainly because of the formation of various volatile by-products including ethanol, acetic acid, propionic acid and butyric acid (Jones *et al.*, 2015), from which H<sub>2</sub> must be purified (Chandrasekhar *et al.*, 2015). Production factors such as tight control of the pH, carbon/nitrogen ratio of the substrate and high temperature requirements add additional challenges and operating costs (Jones *et al.*, 2015; Wang *et al.*, 2012).

### Anoxygenic photo-fermentation

is performed by purple nonsulphur photosynthetic bacteria under anaerobic and anoxic conditions. These organisms use solar energy to convert organic compounds such as organic acids, sugars and glycerol into H<sub>2</sub> and CO<sub>2</sub>. While O<sub>2</sub> sensitivity of the key enzyme, nitrogenase, is not of concern as these bacteria conduct nonoxygenic photosynthesis, the conversion of organic substrates to H<sub>2</sub> appears unlikely to be economical or scalable and the abstraction of these substrates (e.g. sugars) from the food chain is undesirable. Furthermore, H<sub>2</sub> production occurs in the absence of NH<sub>4</sub> due to the high sensitivity of the nitrogenase to nitrogen in the medium. The main challenges of this process are bacterial contamination, substrate type and carbon/nitrogen ratio, synthesis of competing by-products such as polyhydroxybutyrate, sensitivity to temperature and light fluctuations, the low catalytic activity of the nitrogenase, expression suppression by NH<sub>4</sub> (and thus required dilution of waste as a substrate) and lower photochemical efficacy, which collectively lead to low H<sub>2</sub> production levels (Chandrasekhar *et al.*, 2015; Hay *et al.*, 2013).

The bio-H<sub>2</sub> production routes described above have the advantage of being able to utilize carbon sources which would otherwise be lost, for example from waste water, while assisting in waste water management. However, these processes can still be regarded as chemical energy conversion technologies and are not strictly speaking net solar fuel technologies in which the energy from light is captured and stored in the form of fuel.

### Microalgae H<sub>2</sub> systems within a global context

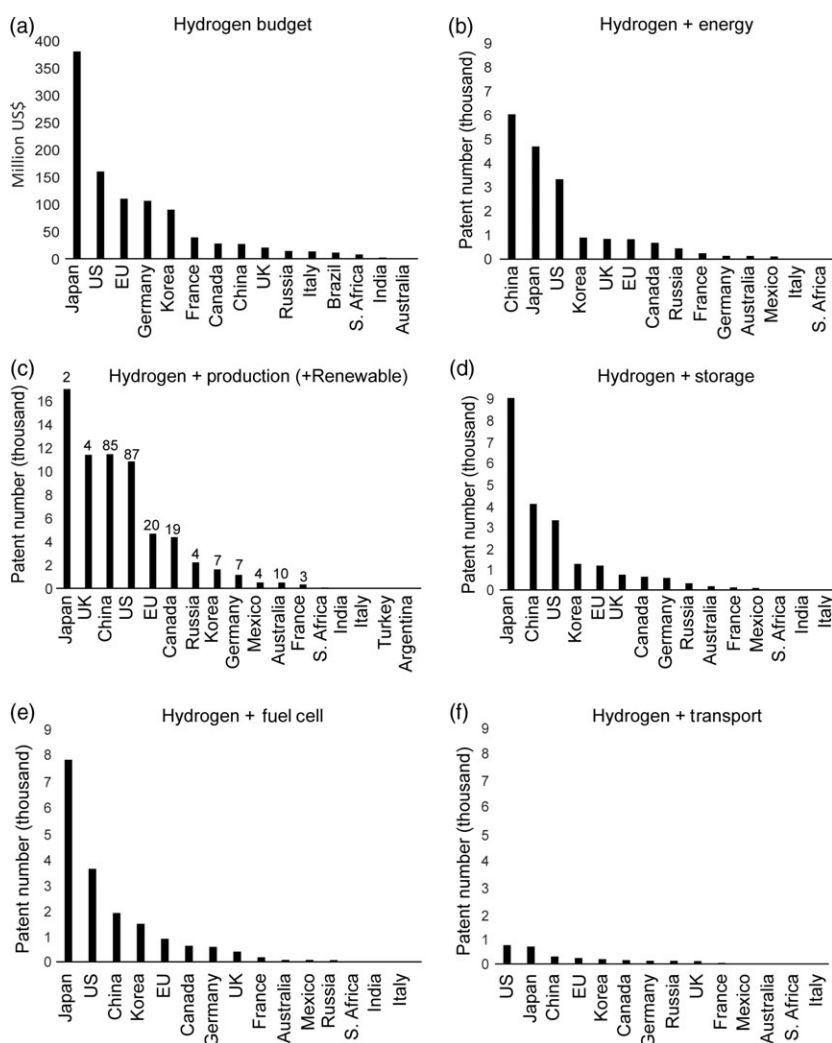
It is also important to understand the global context into which this technology fits, as hydrogen sits at the nexus of several global challenges. In 2010, the G20 nations accounted for 83% of global energy demand and similar levels of CO<sub>2</sub> emissions (BP,

2013). The highest *national* CO<sub>2</sub> emissions levels were reported in China (8 205.9 Mt CO<sub>2</sub>), the US (5 074.1 Mt CO<sub>2</sub>) and India (1 954.0 Mt CO<sub>2</sub>) (IEA, 2014). *Per capita*, CO<sub>2</sub> emissions of each of these G20 nations (2013) range from the highest in Saudi Arabia (~17.2 tCO<sub>2</sub>/year/person) to the lowest in the high 'national emission country' India (1.8 tCO<sub>2</sub>/year/person) (GCP, 2013; PRB, 2013). Not surprisingly, this has resulted in a debate between high (e.g. the US, Saudi Arabia and Australia) and low (such as China and India) *per capita* CO<sub>2</sub> emitters, all of whom are seeking to limit their emission liabilities. Hydrogen as stored chemical energy offers the potential to provide the required *per capita* energy demand without the CO<sub>2</sub> emissions associated with carbon-based fuels. It also offers significant advantages in terms of the development of global distributed systems and networks, as it can be produced using a broad range of technologies making it an important energy currency. However, significant challenges remain. Some of the greatest include market penetration given the dominance of fossil fuels, the high cost of replacing existing carbon-based fuel infrastructure and the technical difficulty of capturing, storing, purifying and compressing H<sub>2</sub> (Bimbo *et al.*, 2013; Hruzewicz-Kolodziejczyk *et al.*, 2012).

In terms of the photosynthetic H<sub>2</sub> production component of this infrastructure, considerable lessons can be learnt from demonstration scale systems for nearer market volatile fuels, for

example ethanol, which are reportedly close to commercial production using cyanobacteria for less than \$2 per gallon (Perkins, 2014). Insights can be gained in terms of capital costs and their potential reduction, strategies to optimize light delivery, as well as methods to capture volatile products as part of a strategy to minimize feedback inhibition.

In terms of H<sub>2</sub> storage and distribution systems, there is as yet no global infrastructure enabling the use of H<sub>2</sub> as a 'drop-in' fuel. Nevertheless, H<sub>2</sub> is widely used in industry and this provides a solid knowledge base to build on (Ramachandran and Menon, 1998). Additionally, during the early stages of deployment, storage and distribution are not critical for the productive use of H<sub>2</sub>, as H<sub>2</sub> can be used to reduce CO<sub>2</sub> to yield a range of CO<sub>2</sub> neutral carbon-based drop-in fuels (Centi and Perathoner, 2009; Wang *et al.*, 2011) compatible with existing storage and distribution systems. Notably, forecasts indicate that by 2025, H<sub>2</sub> may contribute 8–10% to the energy market (Gupta *et al.*, 2013), which provides a development driver for H<sub>2</sub> production, storage, distribution and conversion technologies, and these are actively being developed and deployed internationally (see below). Policies such as tax incentives are also gradually being established (FCHEA, 2014). Consequently, an international movement is beginning to connect solar H<sub>2</sub>-producing technologies with advancements in storage, distribution and fuel cell technologies.



**Fig. 2** Hydrogen budget and potential market in G20 countries. (a): Allocated budget per country for the development of hydrogen technology. (b–f) Patents filed in the respective countries. Numbers derived from the European Espacenet world wide database keyword search using: Hydrogen + Energy, Hydrogen + Production and Hydrogen + Production + Renewable (renewables are shown as absolute patent numbers above bar), Hydrogen + Storage, Hydrogen + Fuel cell, Hydrogen + Transport.



## The patent landscape

Analysis of the global H<sub>2</sub> patent landscape provides valuable insights for a developing microalgal H<sub>2</sub> biotechnology industry, in terms of both challenges and opportunities. National expenditure levels on H<sub>2</sub> technologies by the G20 nations are shown in Figure 2a, with Japan, the US and the EU supporting the largest number of developments. Current patent submissions in the G20 countries in the areas of H<sub>2</sub> energy (Figure 2b) and H<sub>2</sub> production (Figure 2c), as well as renewable H<sub>2</sub> production (Figure 1c, absolute patent numbers given above bar), H<sub>2</sub> storage (Figure 2d), H<sub>2</sub> fuel cells (Figure 2e) and H<sub>2</sub>-driven transport (Figure 2f), highlight the advances in the delivery of these components of a future H<sub>2</sub> economy.

The majority of patents related to H<sub>2</sub> as a renewable energy source were filed in the US and China (Figure 2c; 87 and 85 patents, respectively), countries which are among the highest national CO<sub>2</sub> emitters. Japan reported the highest H<sub>2</sub> fuel cell patent submissions (Figure 2e), consistent with its stated aim of transitioning to a H<sub>2</sub> fuel future (GoJ, 2014). These international patenting patterns may be an indicator of early technology adopter hotspots and highlight the potential of developing renewable H<sub>2</sub> production platforms to supply emerging global H<sub>2</sub> markets and distribution networks.

## Conclusions

Solar-driven microalgal H<sub>2</sub> production is both a promising and challenging biotechnology, and will likely play an important role in the global drive to reduce GHG emissions. Advances in molecular engineering, TEALCA and pilot scale test facilities and predictive design are providing critical tools for the development of the solar fuel systems required to tap into the huge solar resource available to us and which could be used to drive a sustainable energy economy. Using these tools to develop 'deployment ready' microalgae or artificial solar fuel systems in the next 10 years is of critical importance for climate stabilization, but this can only be achieved within a framework of political leadership which will enable up to 70% emission reductions within the next 10–20 year time window.

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